

# Inertial flows in liquid foam microchannels

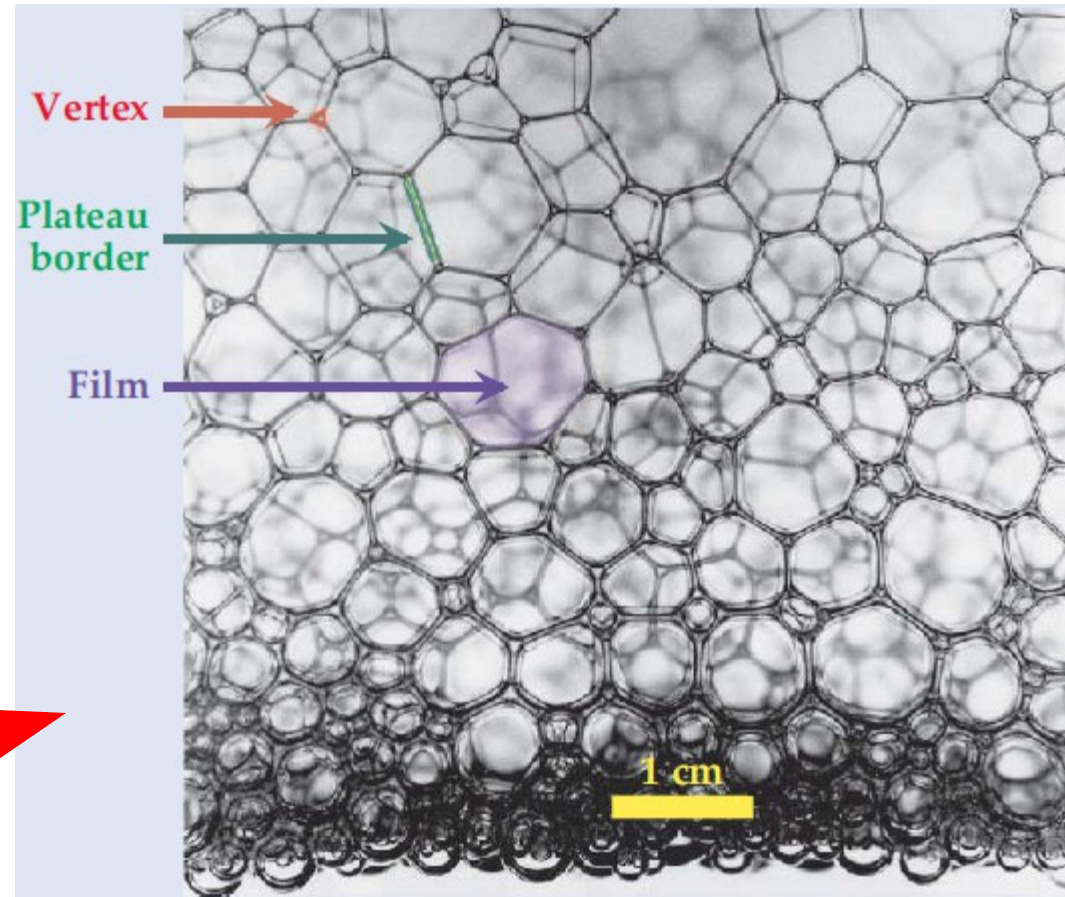
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# Introduction: liquid in foams

## □ Composition

cf: talk by B. Dollet



Durian & Raghavan Phys. Today 2010

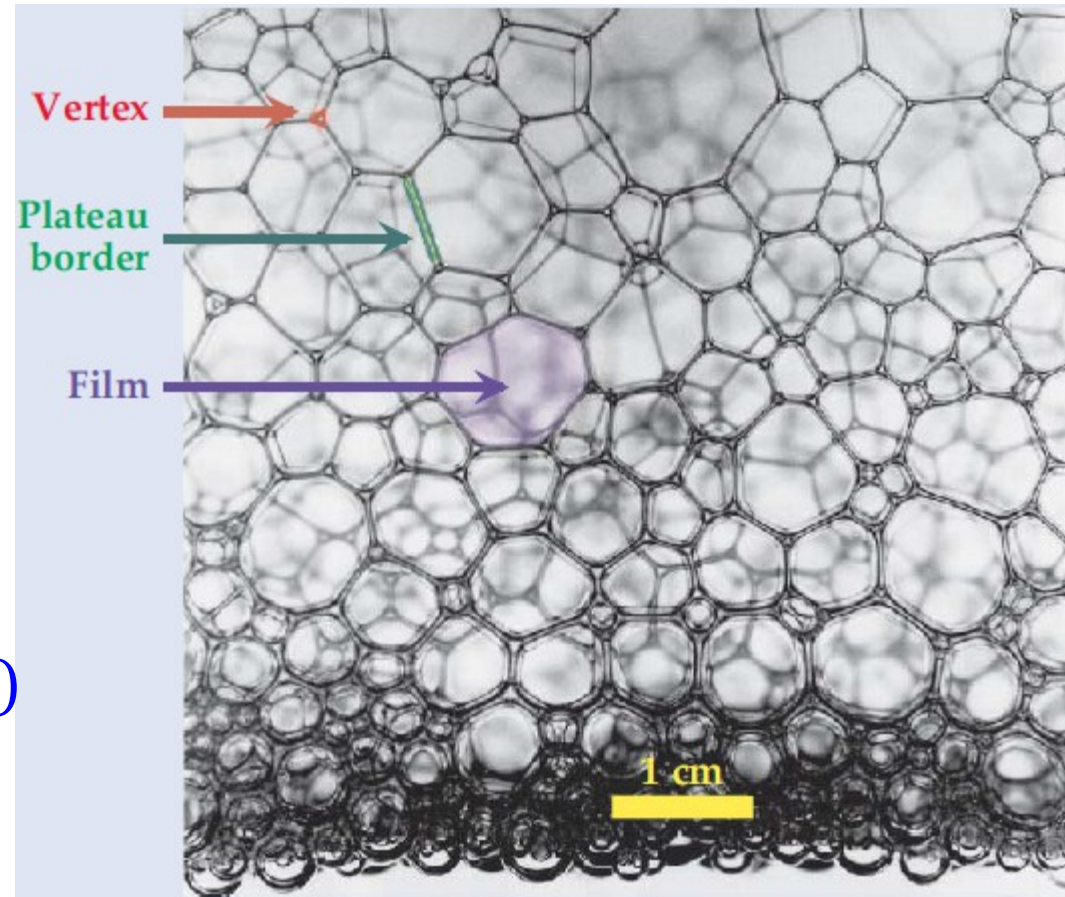
# Introduction: liquid in foams

## □ Composition

dispersion of **gas**  
(bubbles,  $100\mu\text{m}-1\text{cm}$ )

inside liquid phase:

- Plateau Border ( $10-100\mu\text{m}$ )
- vertex
- film ( $10\text{nm}-1\mu\text{m}$ )



Durian & Raghavan Phys. Today 2010

# Motivations

## □ Plateau Border

Liquid microchannel

Held by 3 soap films

Sustained by capillarity

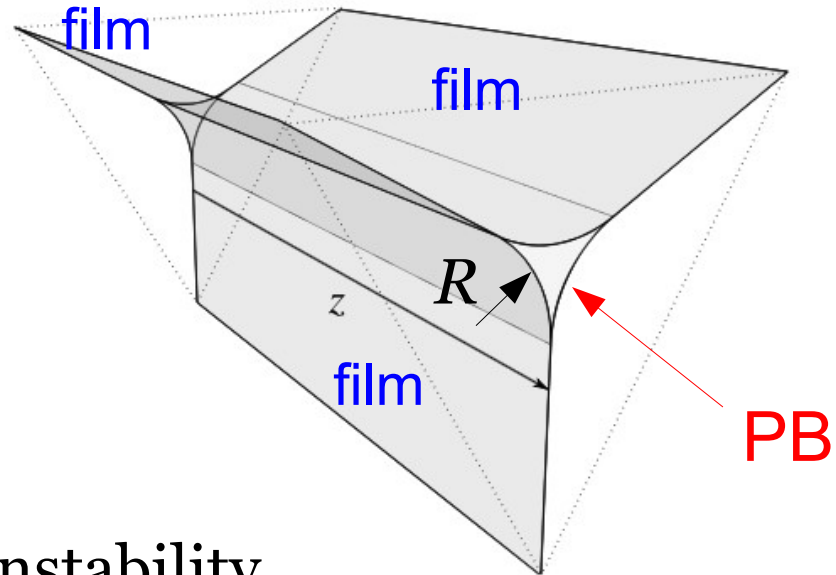
no Rayleigh-Plateau instability

under-pressurized:  $P = P_0 - \gamma/R$

Very flexible and deformable

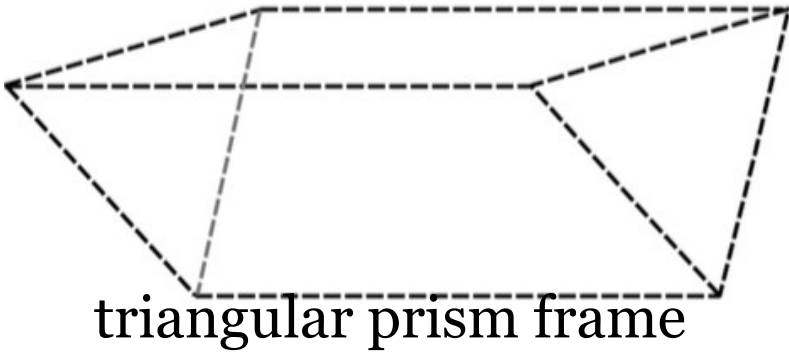
## □ Interest in the mechanical response of a PB (morphologies, flows, ...)

—————▶ Inertial flows at the micron-scale

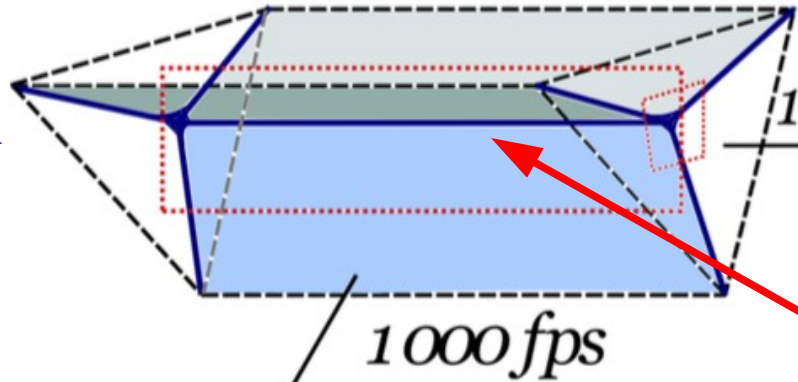
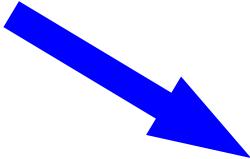


# Setup

□ Single-PB experiment



withdrawn from a surfactant solution



cross-section view



side view

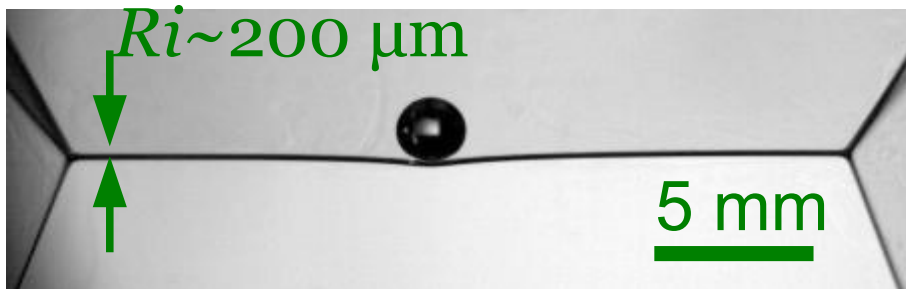


central PB



# I - Drop-injected experiment

- Inertial regime

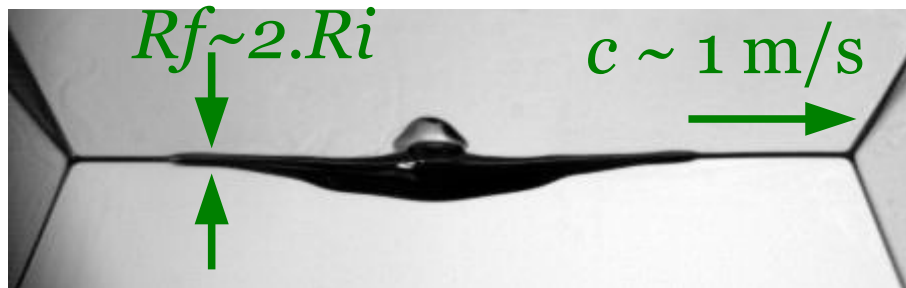
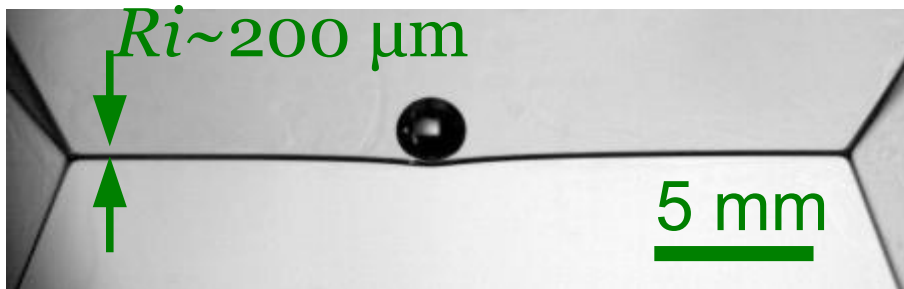


slowed down x100

bulk properties  $\sim$  water  
surface tension  $\gamma \sim 30 \text{ mN/m}$

# I - Drop-injected experiment

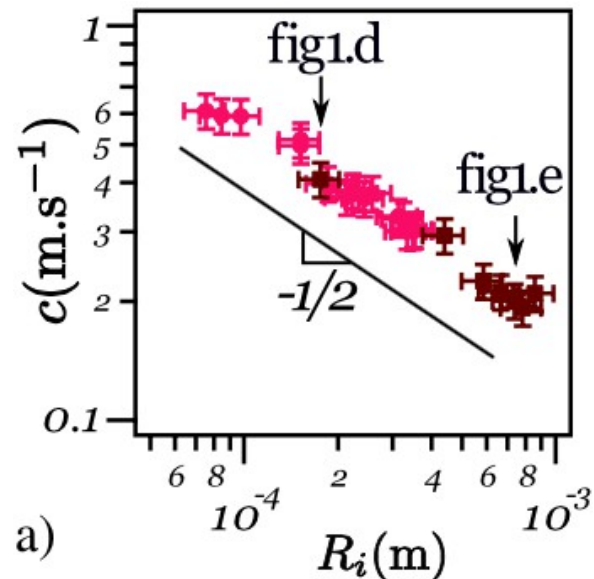
□ Inertial regime



$$\text{Re} = \rho Ri c / \eta \sim 200$$

Capillary hydraulic jump

$$c = (\gamma / \rho Ri)^{-1/2}$$



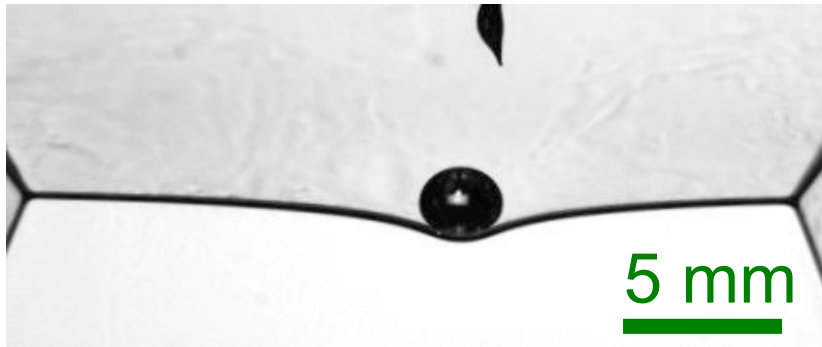
Cohen et al., PRL 2014

Argentina et al., JFM 2015



# I - Drop-injected experiment

## □ Viscous Regime



slowed down x200

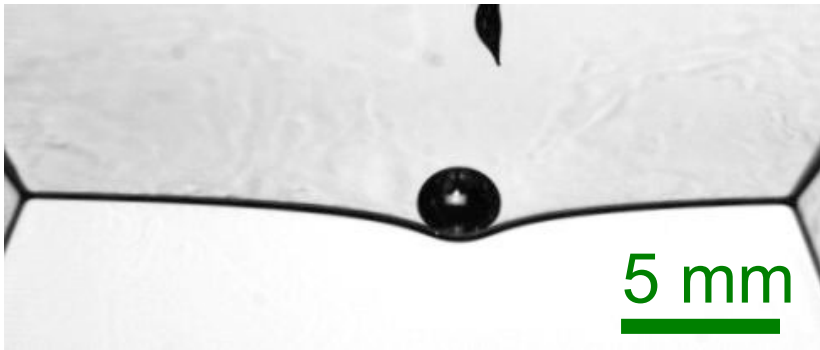
Increasing  $\eta$   
Decreasing  $Ri$

$$Re = \rho Ri c / \eta$$



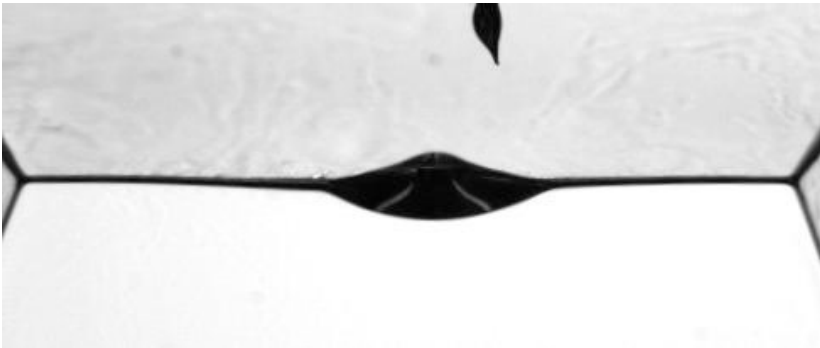
# I - Drop-injected experiment

## □ Viscous Regime



Increasing  $\eta$   
Decreasing  $Ri$

$Re = \rho Ri c / \eta$   
Transition  $Re \sim 20$

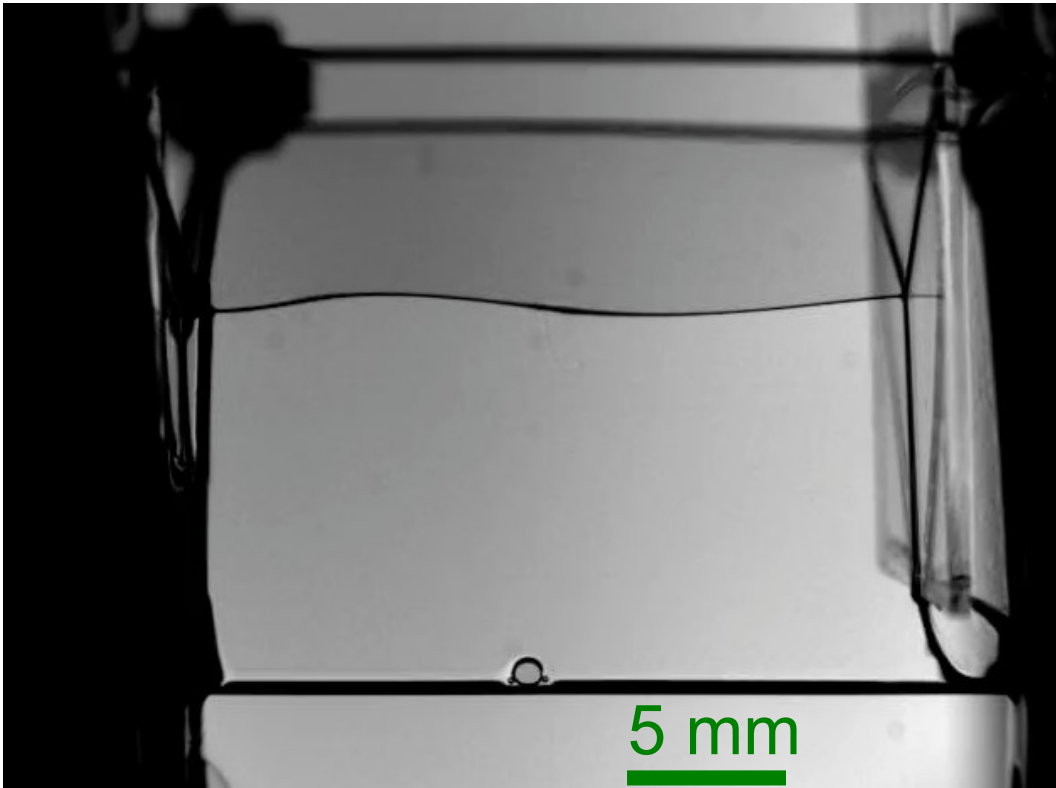


Smooth spreading profile  
Slower dynamics

## II - Oscillation experiment

- Melde's experiment with a liquid string

$$\omega \sim 400 \text{ rad/s}$$

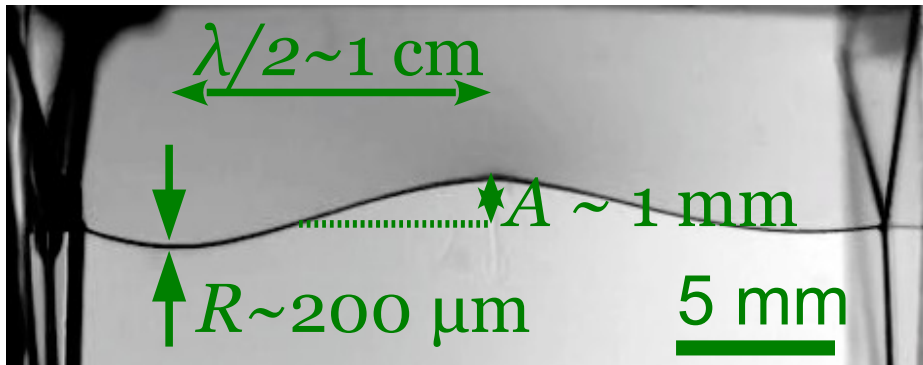


slowed down x100

## II - Oscillation experiment

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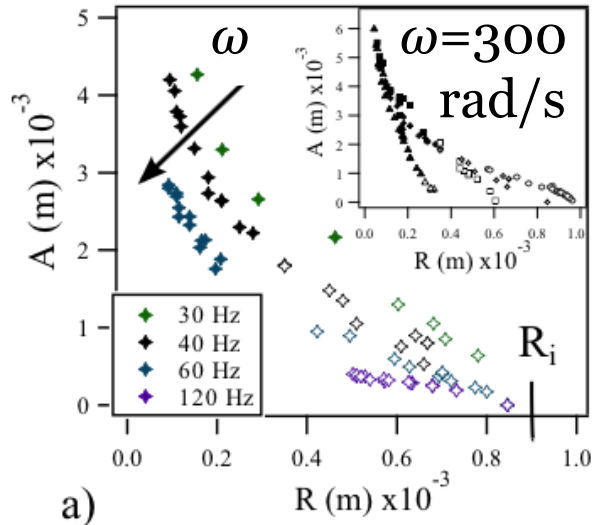
$$\omega \sim 400 \text{ rad/s}$$



Dispersion relation  $\lambda(\omega)$

Inertial regime

$$\text{Re} = \rho R i A \omega / \eta \sim 100$$



1 Bernoulli equation

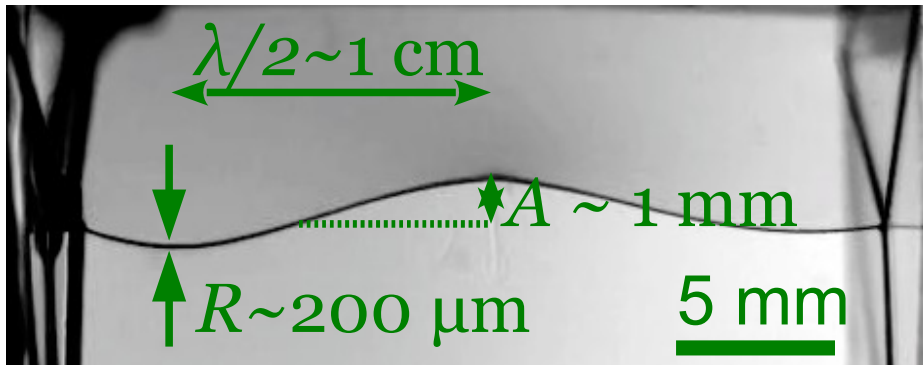
$$\frac{1}{2} \rho \frac{(A\omega)^2}{2} - \frac{\gamma}{R} = - \frac{\gamma}{R_i}$$



## II - Oscillation experiment

□ Melde's experiment with a liquid string

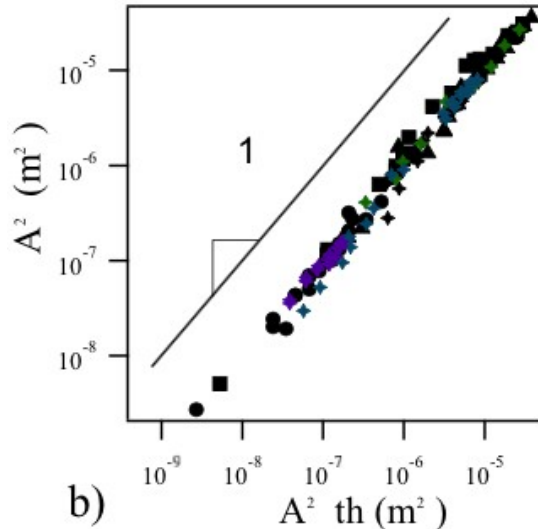
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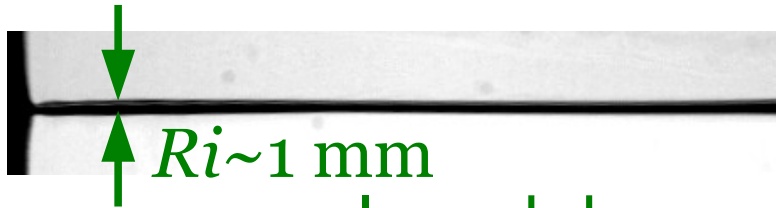
$$\frac{1}{2} \rho \frac{(A\omega)^2}{2} - \frac{\gamma}{R} = - \frac{\gamma}{R_i}$$

$A \nearrow$

$R \searrow$

## II - Oscillation experiment

- Melde's experiment with a liquid string



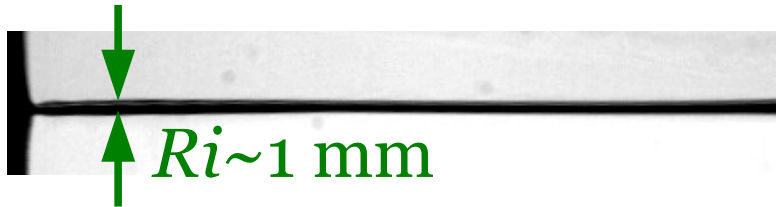
High amplitude regime

$R_i \sim 1 \text{ mm}$

slowed down x20

## II - Oscillation experiment

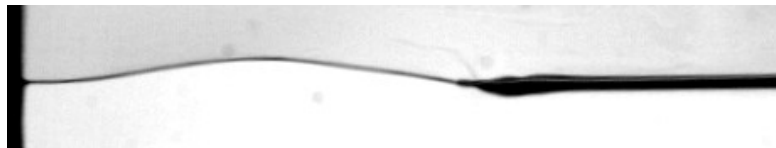
- Melde's experiment with a liquid string



High amplitude regime



Bernoulli  
Non-linear effects



Transition to a bi-sized system

# Conclusion

- Inertial flows at the microchannel scale
- Non-linear effects and specific morphologies
- Coupling with the three holding films